

PATENT
13002.0071.NPUS00

APPLICATION FOR UNITED STATES LETTERS PATENT

for

**FUNCTIONALIZED VEGETABLE OIL DERIVATIVES,
LATEX COMPOSITIONS AND COATINGS**

by

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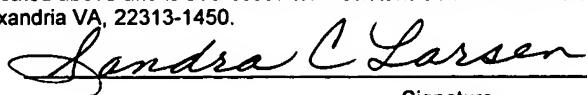
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BACKGROUND OF THE INVENTION

The present invention is directed to vegetable oil derivatives. More particularly, the present invention is directed to functionalized vegetable oil derivatives that can be used in latexes and coatings.

5 One problem encountered by coatings manufacturers is the development of
6 formulations containing low VOC-coalescing aids or plasticizers. For instance, emulsion
7 polymers are currently formulated with coalescing aids or plasticizers in order to form
8 films at and below ambient conditions yet dry to films of sufficient glass transition
9 temperature (T_g) to perform adequately at and above room temperature. In general, the
10 ability of emulsion polymers to form or coalesce into film is governed by the minimum
11 film forming temperature (MFT) of the polymer in question. Low MFT polymers are
12 required in order to exhibit coalescence, flow, and surface wetting properties. However,
13 if the polymer remains soft and tacky, the coatings are not usable. Therefore, it is
14 necessary to develop a technology in which coating formulations contain suitable
15 ingredients to provide an initial low MFT, which, upon application, form nontacky,
16 durable, hard, and water resistant surfaces having a T_g significantly above their MFT.

17 Various other coating compositions which cure under ambient conditions are
18 known in the prior art. A few such examples involve curing by a chemical reaction such
19 as epoxide-carboxylic acid reaction, isocyanate-moisture reaction, polyaziridine-
20 carboxylic acid reaction, and activated methylene-unsaturated acrylic reaction.

Recently, a number of new latex or emulsion compositions derived from semi-drying and/or non-drying oils have been developed for use in coatings, adhesives and inks. Such compositions are disclosed in U.S. Patents Nos. 6,001,913; 6,174,948; and 6,203,720 each of which is incorporated herein by reference in its entirety.

25 The search for additional compositions that can be used in latexes and coatings is
26 continuing. Accordingly, it would be an advancement in the art to provide compositions
27 that can be made from renewable resources that are suitable for use in latexes and
28 coatings.

SUMMARY OF THE INVENTION

30 The present invention is directed to functionalized vegetable oil derivatives which
31 are useful in latexes and coatings. In the preferred embodiment, an ethylenically

1 unsaturated vegetable oil is modified by the addition of an enophile or dienophile having
2 an acid, ester or anhydride functionality. The modified vegetable oil is then reacted with a
3 functional vinyl monomer to form the vegetable oil derivative. Suitable monomers
4 include hydroxy, amine, thiol, oxirane vinyl monomers.

5 The functionalized vegetable oil derivatives can be formulated into latexes and
6 other coating compositions.

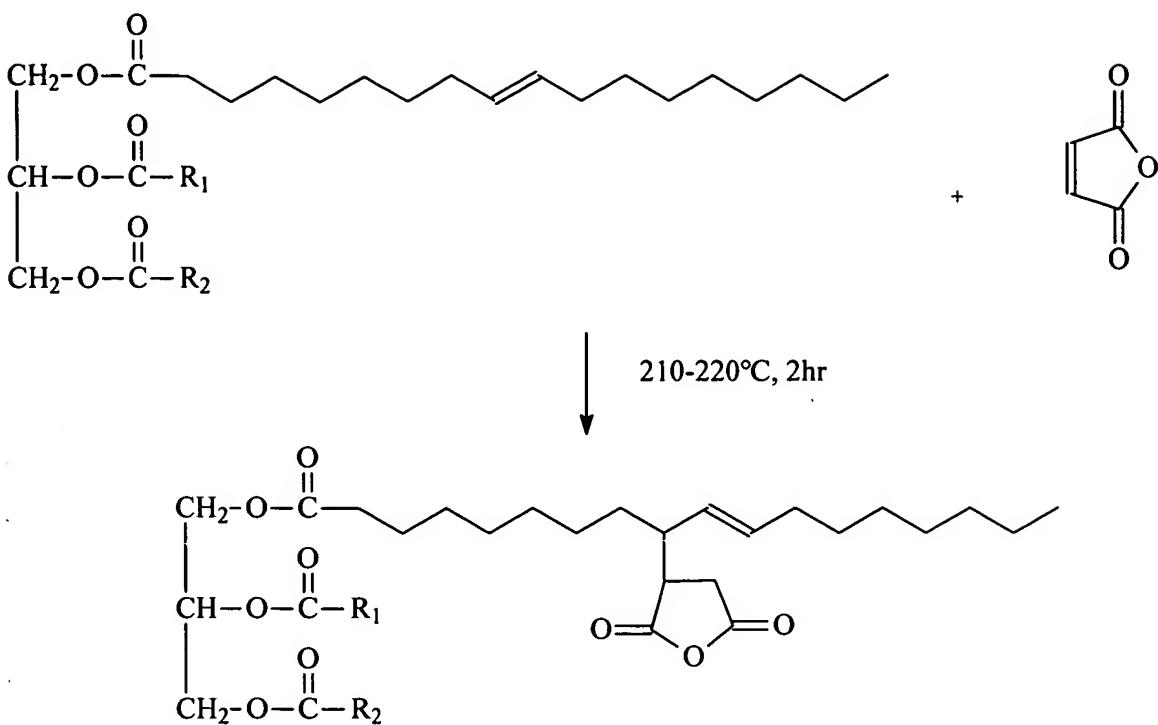
7 **DETAILED DESCRIPTION OF THE PREFERRED EMBODIMENTS**

8 The present invention is directed to a series of vegetable oil macromonomers and
9 their use in latexes and coatings. The invention is also directed to the method of
10 producing these macromonomers. This set of monomers is derived by reacting
11 unsaturated vegetable oils with an enophile or dienophile having an acid, ester or
12 anhydride functionality, and then reacting the derivative with a suitable hydroxy, amine,
13 thiol, oxirane, or other functional vinyl monomer.

14 In a preferred embodiment, an unsaturated vegetable oil, such as soybean oil is
15 reacted with maleic anhydride to form a maleinized vegetable oil as schematically shown
16 in Reaction 1. Preferably, the reaction is performed at a temperature of about 200 °C to
17 about 240 °C. More preferably, the reaction is performed at a temperature of about 210
18 °C to about 220 °C.

19

1 **Reaction 1:**



6 Any unsaturated vegetable oil can be used in the present invention. However,
7 linseed oil, soybean oil and sunflower oil are preferred.

8 Many different compounds can be used to modify the unsaturated vegetable oil.
9 They include enophiles and dienophiles that contain acid, ester or anhydride
10 functionality. Examples include but are not limited to maleic anhydride, fumaric acid,
11 itaconic anhydride and maleate esters.

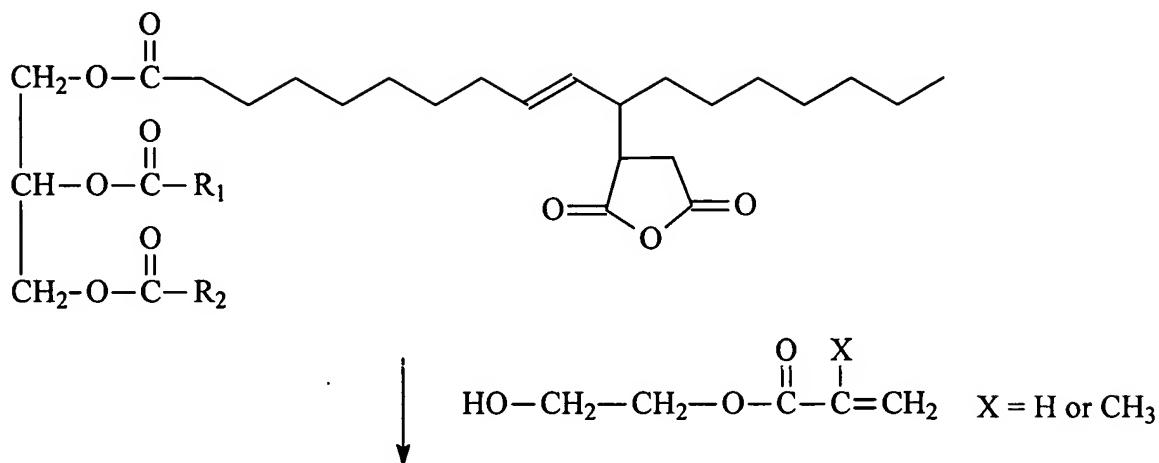
12 The modified vegetable oil is then reacted with a suitable functional vinyl
13 monomer to form the macromonomers of the present invention. A series of exemplary
14 reactions are illustrated in Reactions 2a-2e. In Reaction 2a, the maleinized vegetable oil
15 is reacted with hydroxyethyl acrylate (HEA) or hydroxyethyl methacrylate (HEMA). In
16 Reaction 2b, the maleinized vegetable oil is reacted with 2-(tert-butylamino)ethyl
17 methacrylate (BAEMA). In Reaction 2c, the maleinized vegetable oil is reacted with
18 glycidyl acrylate (GA) or glycidyl methacrylate (GMA). In Reaction 2d, the maleinized
19 vegetable oil is reacted with allyl amine. Finally, in Reaction 2e, the maleinized

1 vegetable oil is reacted with a vinyl ether such as hydroxybutyl vinyl ether where R is
2 $-(\text{CH}_2)_4-$.

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4 **Reaction 2a**

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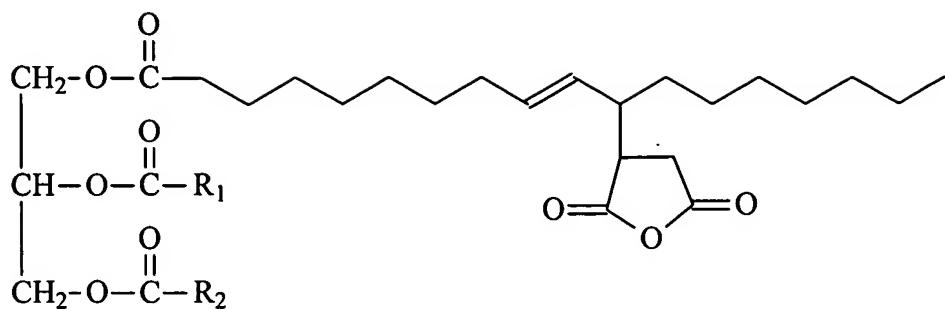
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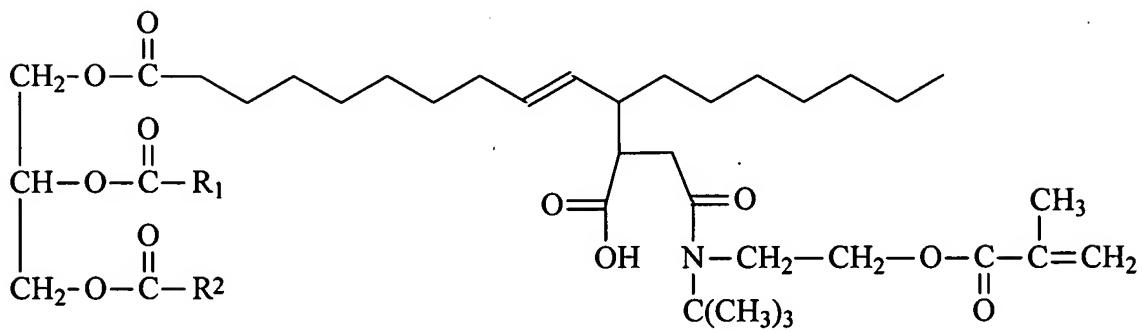
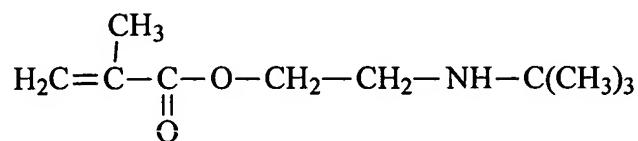
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1 **Reaction 2b**

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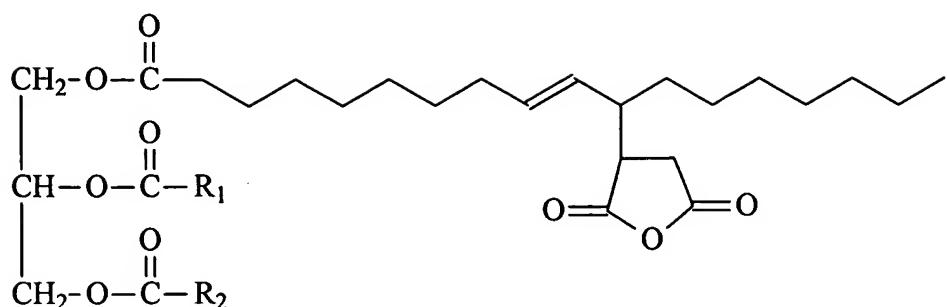
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1 **Reaction 2c**

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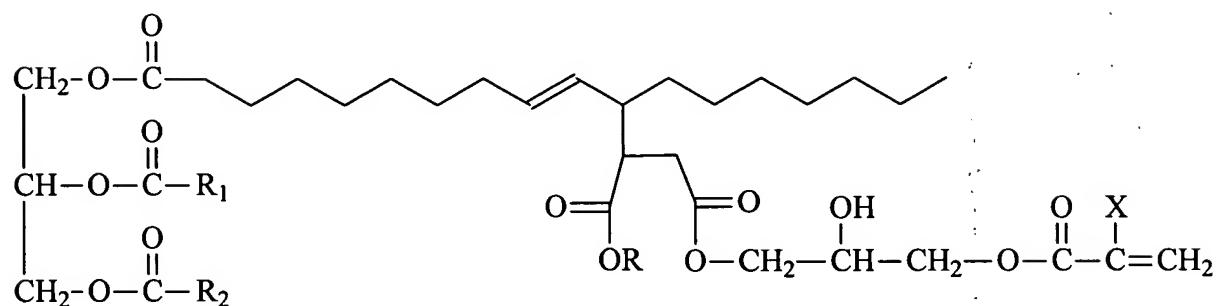
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1. HO-R

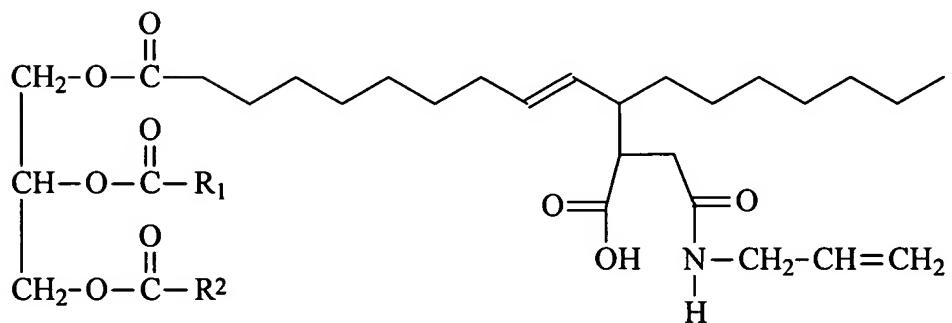
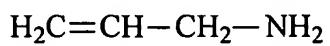
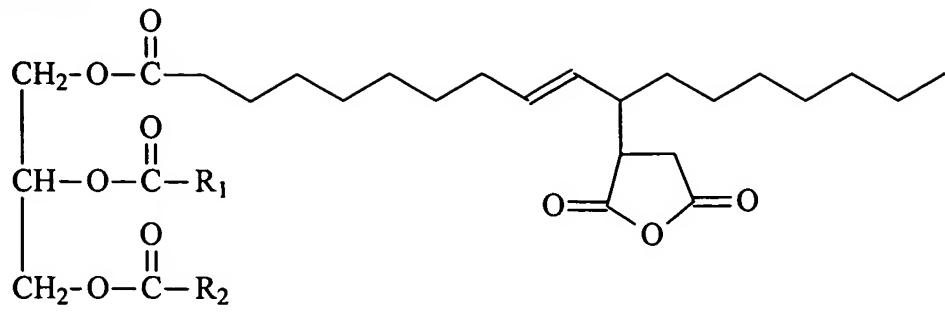
2. $\text{H}_2\text{C}-\text{CH}(\text{O})-\text{CH}_2-\text{O}-\text{C}(=\text{O})-\text{C}(=\text{CH}_2)\text{X}$ $\text{X} = \text{H or CH}_3$



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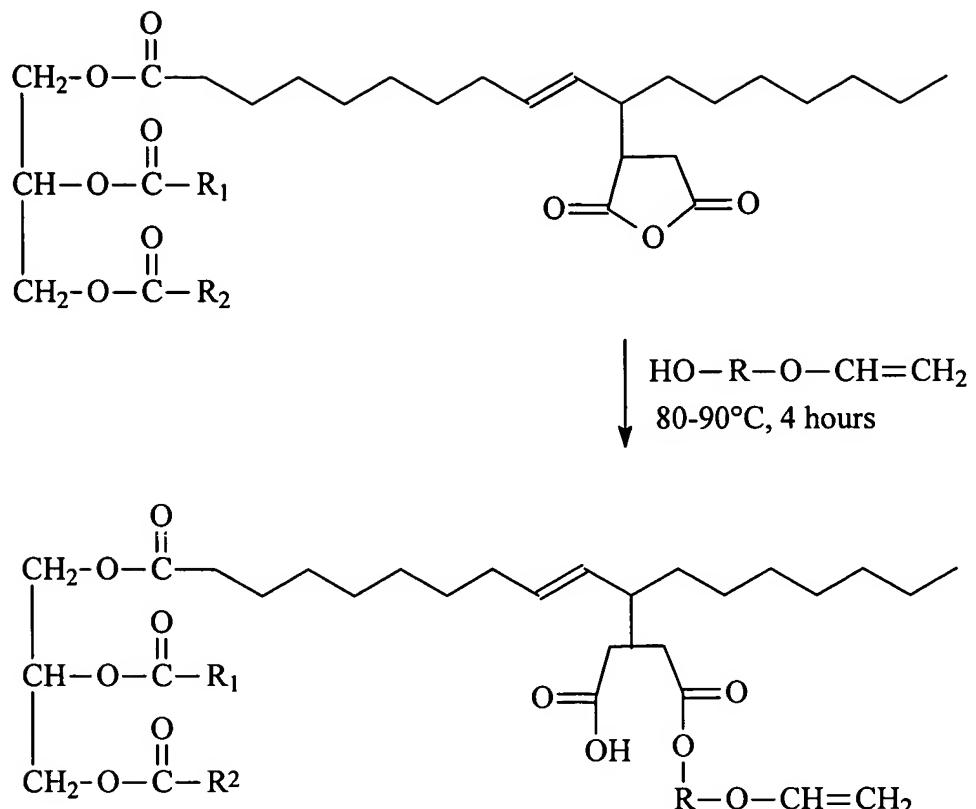
Reaction 2d



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1 **Reaction 2e**

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1 Examples of additional functionalized vinyl monomers that can be used in the
2 present invention include, but are not limited to, hydroxypropyl acrylate, hydroxypropyl
3 methacrylate, hydroxybutyl acrylate, hydroxybutyl methacrylate, allyl alcohol, 3-butanol,
4 acrylamide and methacrylamide.

5 The macromonomers of the present invention can be used to make latexes and
6 coatings compositions. In the preferred embodiment, the latexes are formed in a staged
7 polymerization process as disclosed in published U.S. Application 2003/0045609, the
8 teachings of which are hereby incorporated by reference. However, non-staged latex
9 polymerization processes can also be used.

10 The modified vegetable oils of the present invention can then be copolymerized
11 with conventional functionalized monomers in emulsion polymerization processes to
12 produce vinyl polymers.

13 The invention is further understood by reference to the following examples which
14 describe the formation of various macromonomers as well as the formulation of latexes
15 and coatings.

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Example 1

20 Soybean oil (51.03 kg) was heated in a reactor to 100°C, and nitrogen gas was
21 passed through the reaction mixture to remove the oxygen in the system. Maleic
22 anhydride (14.17 kg) and xylene (2.93 mL) were added and the temperature was slowly
23 raised to 205-210°C and held for 2.5 hours. The maleic anhydride concentration was
24 followed via gas chromatography (GC). Heating was stopped when the maleic anhydride
25 concentration reached 1-2%, and the reaction mixture was cooled to 90°C.

26 Phenothiazine (86 g) was mixed with hydroxyethyl acrylate (13.30 kg) and added
27 to the reactor. Next, 86 g of phosphoric acid (85% solution in water) was added to the
28 reaction mixture. The temperature was raised to 110-115°C and heating was continued
29 for 2.5 hours. Heating was stopped when the hydroxyethyl acrylate concentration
30 dropped below 4% (determined by GC). The reaction mixture was cooled to 60-70°C
31 and the reaction product, monomer 'A' was discharged.

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Example 2

Maleic anhydride (48 g) was mixed with linseed oil (152 g) and nitrogen gas was passed through the reaction mixture to remove the oxygen in the system. The reaction mixture was heated to 150°C over 30 minutes and then heated to 200°C where it was held for 2.5 hours. The reaction mixture was cooled to 50°C, and hydroxyethyl acrylate (58 g), phenothiazine (0.25 g), and phosphoric acid, 85% solution in water (0.25 g) were added to the reaction mixture. The reaction was continued for 3-5 hours at 80°C till all the hydroxyethyl acrylate had reacted to yield monomer 'B'.

Example 3

12 Maleic anhydride (72 g) was mixed with soybean oil (221 g) and nitrogen gas was
13 passed through the reaction mixture to remove the oxygen in the system. The reaction
14 mixture was heated to 150°C over 30 minutes and then heated to 200°C where it was held
15 for 2.5 hours. The reaction mixture was cooled to 50°C, and hydroxyethyl methacrylate
16 (105 g), phenothiazine (0.25 g), and 1-methyl imidazole (0.30 g) were added to the
17 reaction mixture. The reaction was continued for 3-5 hours at 110°C till all the
18 hydroxyethyl acrylate had reacted to yield monomer ‘C’.

Example 4

22 Maleic anhydride (46 g) was mixed with linseed oil (215 g) and nitrogen gas was
23 passed through the reaction mixture to remove the oxygen in the system. The reaction
24 mixture was heated to 150°C over 30 minutes and then heated to 200°C where it was held
25 for 2.5 hours. The reaction mixture was cooled to 50°C, and hydroxyethyl acrylate (61
26 g), phenothiazine (0.25 g), and phosphoric acid, 85% solution in water (0.3 g) were added
27 to the reaction mixture. The reaction was continued for 3-5 hours at 110°C till all the
28 hydroxyethyl acrylate had reacted to yield monomer 'D'.

Example 5

Maleic anhydride (477 g) was mixed with soybean oil (2150 g) and nitrogen gas was passed through the reaction mixture to remove the oxygen in the system. The reaction mixture was heated to 150°C over 30 minutes and then heated to 215°C where it was held for 2 hours. The reaction mixture was cooled to 90°C, and hydroxyethyl acrylate (565 g), phenothiazine (5 g), and phosphoric acid, 85% solution in water (5 g) were added to the reaction mixture. The reaction was continued for 4-5 hours at 110°C till all the hydroxyethyl acrylate had reacted to yield monomer 'E'.

Example 6

Soybean oil (51.03 kg) was heated in a reactor to 100°C, and nitrogen gas was passed through the reaction mixture to remove the oxygen in the system. Maleic anhydride (11.21 kg) and xylene (2.93 mL) were added and the temperature was slowly raised to 205-210°C and held for 2.5 hours. The maleic anhydride concentration was followed via GC. Heating was stopped when the maleic anhydride concentration reached 1-2%, and the reaction mixture was cooled to 90°C.

Phenothiazine (50 g) was mixed with hydroxyethyl acrylate (8.99 kg) and added to the reactor. Next, 81 g of phosphoric acid (85% solution in water) was added to the reaction mixture. The temperature was raised to 120°C and heating was continued for 2.5 hours. Heating was stopped when the hydroxyethyl acrylate concentration dropped below 4% (determined by GC). The reaction mixture was cooled to 60-70°C and the reaction product, monomer 'F', was discharged.

Example 7

Linseed oil (51.03 kg) was heated in a reactor to 100°C, and nitrogen gas was passed through the reaction mixture to remove the oxygen in the system. Maleic anhydride (11.21 kg) and xylene (2.93 mL) were added and the temperature was slowly raised to 205-210°C and held for 2.5 hours. The maleic anhydride concentration was followed via GC. Heating was stopped when the maleic anhydride concentration reached 1-2%, and the reaction mixture was cooled to 90°C.

Phenothiazine (50 g) was mixed with hydroxyethyl acrylate (8.99 kg) and added to the reactor. Next, 81 g of phosphoric acid (85% solution in water) was added to the

1 reaction mixture. The temperature was raised to 120°C and heating was continued for 2.5
2 hours. Heating was stopped when the hydroxyethyl acrylate concentration dropped
3 below 4% (determined by GC). The reaction mixture was cooled to 60-70°C and the
4 reaction product, monomer 'G', was discharged.

5 **Example 8**

6 Soybean oil (981 g) was heated in a reactor to 100°C, and nitrogen gas was
7 passed through the reaction mixture to remove the oxygen in the system. Maleic
8 anhydride (323 g) and xylene (1 drop) were added and the temperature was slowly raised
9 to 205-210°C and held for 4.5 hours. The maleic anhydride concentration was followed
10 via GC. Heating was stopped when the maleic anhydride concentration reached 1-2%,
11 and the reaction mixture was cooled to 90°C.

12 Phenothiazine (1.35 g) was mixed with hydroxyethyl acrylate (253 g) and added to
13 the reactor. Next, 1.54 g of phosphoric acid (85% solution in water) was added to the
14 reaction mixture. The temperature was raised to 120°C and heating was continued for 3
15 hours. The reaction mixture was cooled to 60-70°C and the reaction product, monomer
16 'H', was discharged.

17 **Example 9**

18 Soybean oil (981 g) was heated in a reactor to 100°C, and nitrogen gas was
19 passed through the reaction mixture to remove the oxygen in the system. Maleic
20 anhydride (323 g) and xylene (1 drop) were added and the temperature was slowly raised
21 to 205-210°C and held for 4.5 hours. The maleic anhydride concentration was followed
22 via GC. Heating was stopped when the maleic anhydride concentration reached 1-2%,
23 and the reaction mixture was cooled to 90°C.

24 Phenothiazine (1.35 g) was mixed with hydroxyethyl methacrylate (305 g) and
25 added to the reactor. Next, 1-methyl imidazole (1.54 g) was added to the reaction
26 mixture. The temperature was raised to 120°C and heating was continued for 3 hours.
27 The reaction mixture was cooled to 60-70°C and the reaction product, monomer 'I', was
28 discharged.

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Example 10

Linseed oil (152 g) was heated in a reactor to 100°C, and nitrogen gas was passed through the reaction mixture to remove the oxygen in the system. Maleic anhydride (48 g) and xylene (1 drop) were added and the temperature was slowly raised to 205-210°C and held for 4.5 hours. The maleic anhydride concentration was followed via GC. Heating was stopped when the maleic anhydride concentration reached 1-2%, and the reaction mixture was cooled to 90°C.

Phenothiazine (0.5 g) was mixed with hydroxyethyl methacrylate (75 g) and added to the reactor. Next, 0.5 g of phosphoric acid (85% solution in water) was added to the reaction mixture. The temperature was raised to 100°C and heating was continued for 4-5 hours. The reaction mixture was cooled to 60-70°C and the reaction product monomer 'J', was discharged.

Example 11

17 Sunflower oil (52.6 kg) was heated in a reactor to 100°C, and nitrogen gas was
18 passed through the reaction mixture to remove the oxygen in the system. Maleic
19 anhydride (11.57 kg) was added and the temperature was slowly raised to 205-210°C and
20 held for 2.5 hours. The maleic anhydride concentration was followed via GC. Heating
21 was stopped when the maleic anhydride concentration reached 1-2%, and the reaction
22 mixture was cooled to 90°C.

23 Phenothiazine (125 g) was mixed with hydroxyethyl acrylate (13.69 kg) and
24 added to the reactor. Next, 125 g of phosphoric acid (85% solution in water) was added
25 to the reaction mixture. The temperature was raised to 100°C and heating was continued
26 for 4-5 hours. The reaction mixture was cooled to 60-70°C and the reaction product
27 monomer 'K' was discharged.

Example 12

Maleic anhydride (48 g) was mixed with sunflower oil (152 g) and nitrogen gas was passed through the reaction mixture to remove the oxygen in the system. The reaction mixture was heated to 150°C over 30 minutes and then heated to 200°C where it was held for 2.5 hours. The reaction mixture was cooled to 50°C, and hydroxyethyl

1 acrylate (58 g), phenothiazine (0.25 g), and phosphoric acid, 85% solution in water (0.25
2 g) were added to the reaction mixture. The reaction was continued for 3-5 hours at 80°C
3 till all the hydroxyethyl acrylate had reacted to yield monomer 'L'.

4 **Example 13**
5

6 Maleic anhydride (49 g) was mixed with soybean oil (221 g) and nitrogen gas was
7 passed through the reaction mixture to remove the oxygen in the system. The reaction
8 mixture was heated to 150°C over 30 minutes and then heated to 200°C where it was held
9 for 2.5 hours. The reaction mixture was cooled to 50°C, and styrene (100 g), and allyl
10 amine (28 g) were added to the reaction mixture. The reaction was continued for 5 hours
11 at 50°C to yield monomer 'M'.

12 **Example 14**
13

14 Maleic anhydride (49 g) and 2-methylmercaptopbenzoylthiazole (0.1 g) were
15 mixed with soybean oil (221 g) and nitrogen gas was passed through the reaction mixture
16 to remove the oxygen in the system. The reaction mixture was heated to 150°C over 30
17 minutes and then heated to 215°C where it was held for 2.5 hours. The reaction mixture
18 was cooled to 70°C, and phenothiazine (0.35 g), and 2-(*tert*-butyl amino) ethyl
19 methacrylate (92 g) were added to the reaction mixture. The reaction was continued for 5
20 hours at 80°C to yield monomer 'N'.

22 **Example 15**
23

24 Maleic anhydride (49 g) and 2-methylmercaptopbenzoylthiazole (0.1 g) were
25 mixed with soybean oil (221 g) and nitrogen gas was passed through the reaction mixture
26 to remove the oxygen in the system. The reaction mixture was heated to 150°C over 30
27 minutes, and then heated to 215°C where it was held for 2.5 hours. The reaction mixture
28 was cooled to 90°C, and water (27 g) was added to the reaction mixture. The reaction
29 was continued for 2.5 hours at 95°C. Then phenothiazine (0.35 g), glycidyl acrylate (128
30 g), and tetramethylammonium chloride (1 g) were added. The reaction was continued for
31 4 hours at 100°C to yield monomer 'O'.

33

Example 16

3 Maleic anhydride (49 g) and xylene (0.1 g) were mixed with soybean oil (221 g)
4 and nitrogen gas was passed through the reaction mixture to remove the oxygen in the
5 system. The reaction mixture was heated to 150°C over 30 minutes and then heated to
6 215°C where it was held for 2.5 hours. The reaction mixture was cooled to 90°C, and
7 poly(ethylene glycol)monomethyl ether (140 g) and 1-methylimidazole (0.5 g) were
8 added to the reaction mixture. The reaction was continued for 2.5 hours at 130°C. Next,
9 phenothiazine (0.35 g), glycidyl methacrylate (56.8 g), and tetramethylammonium
10 chloride (1 g) were added. The reaction was continued for 4 hours at 100°C to yield
11 monomer ‘P’.

Example 17

15 Soybean oil (981 g) was heated in a reactor to 100°C, and nitrogen gas was
16 passed through the reaction mixture to remove the oxygen in the system. Maleic
17 anhydride (197 g) and 2-mercaptopbenzothiazole (0.363 g) were added and the
18 temperature was slowly raised to 215-220°C and held for 2.5 hours. The maleic
19 anhydride concentration was followed via GC. Heating was stopped when the maleic
20 anhydride concentration reached 1-2%, and the reaction mixture was cooled to 90°C.

21 Phenothiazine (1.35 g) was mixed with hydroxybutyl vinyl ether (233 g) and
22 added to the reactor. Next, 1-methyl imidazole (1.54 g) was added to the reaction
23 mixture. The temperature was raised to 100°C and heating was continued for 2 hours.
24 The reaction mixture was cooled to 60-70°C and the reaction product, monomer 'Q' was
25 discharged.

Example 18

Latex synthesis

29 The first stage pre-emulsion was prepared by dissolving 0.005 lb (2.27 g) of
30 Rhodapex CO 436, and 0.002 lb (0.91 g) of Igepal® CO-887 in 0.78 lb (353.38 g) of
31 deionized water. Next, 0.072 lb (32.65 g) of butyl acrylate, 0.056 lb (25.40 g) of methyl
32 methacrylate, and 0.0014 lb (0.64 g) of methacrylic acid was added and the mixture was

1 stirred at high speed for 20 minutes. The initiator solution was prepared by dissolving
2 0.02 lb (9.07 g) of ammonium persulfate in 0.177 lb (80.29 g) of deionized water.

3 The second stage pre-emulsion was prepared by dissolving 0.0146 lb (6.62 g) of
4 sodium bicarbonate, 0.092 lb (41.73 g) of Rhodapex® CO-436, and 0.034 lb (15.42 g) of
5 Igepal CO-887 in 1.48 lb (671.32 g) of deionized water. Next, 1.34 lb (607.81 g) of butyl
6 acrylate, 1.064 lb (482.62 g) of methyl methacrylate, 0.03 lb (13.61 g) of methacrylic
7 acid, 0.03 lb (13.61 g) of divinyl benzene, and 0.15 lb (68.25 g) of monomer 'F' were
8 added, and stirred for 5 minutes. An aqueous solution of diacetone acrylamide was
9 prepared by dissolving diacetone acrylamide (0.117 lb, 53.07 g) in deionized water
10 (0.132 lb, 59.87 g) and added to the pre-emulsion and stirred for 20 minutes at high
11 agitation.

12
13 A 1-gallon reactor was charged with 0.97 lb (439.98 g) of deionized water and
14 0.01 lb (4.54 g) of Rhodapex CO-436. The mixture was stirred well, purged with
15 nitrogen for 15 minutes, and heated to 80 ± 2 °C. The first stage pre-emulsion solution
16 and 0.035 lb (15.87 g) of the initiator solution were added to the reactor. 15 minutes
17 later, the second stage pre-emulsion, and the remaining initiator solution are fed into the
18 reactor at constant rate over 2.75 hours and 3.0 hours, respectively.

19 An oxidizer solution was prepared by dissolving 0.0032 lb (1.45 g) of *t*-butyl
20 hydroperoxide in 0.026 lb (11.79 g) of deionized water. A reducer solution was prepared
21 by dissolving 0.003 lb (1.36 g) of sodium metabisulfite in 0.026 lb (11.79 g) of deionized
22 water. The oxidizer and reducer solutions were charged to the reactor simultaneously
23 over 1.5 hours at a constant rate. The reactor was held at the same temperature for
24 another 30 minutes and cooled over 45 minutes to 35°C. Next, 0.57 lb (258.55 g) of
25 ammonia was added slowly under stirring.

26 In another container, 0.059 lb (26.76 g) of adipic dihydrazide was dissolved in
27 0.06 lb (27.21 g) of deionized water, and added slowly to the latex under stirring. Lastly,
28 the latex was filtered through a 100 mesh filter.

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Example 19

Latex synthesis (continued)

5 Latexes with varying percentages of monomer 'F' were synthesized as follows. A
6 latex without any vegetable oil monomer was synthesized and used as the control.

| | 2% Monomer 'F' | 4% Monomer 'F' | 6% Monomer 'F' | Control |
|-----------------------|-------------------|-------------------|-------------------|--------------|
| Kettle Charge | | | | |
| Deionized water | 110.0 | 110.0 | 110.0 | 110.0 |
| Rhodapex CO-436 | 1.2 | 1.2 | 1.2 | 1.2 |
| | | | | |
| Stage I | | | | |
| Deionized water | 166.9 | 166.9 | 166.9 | 166.9 |
| Sodium bicarbonate | 1.7 | 1.7 | 1.7 | 1.7 |
| Rhodapex CO-436 | 10.4 | 10.4 | 10.4 | 10.4 |
| Igepal CO-887 | 3.8 | 3.8 | 3.8 | 3.8 |
| Butyl acrylate | 165.0 | 160.0 | 156.0 | 169.0 |
| Methyl methacrylate | 123.0 | 121.0 | 120.0 | 125.0 |
| Divinyl benzene | 6.6 | 6.6 | 6.6 | 6.6 |
| Methacrylic acid | 3.2 | 3.2 | 3.2 | 3.2 |
| Diacetone acrylamide | 13.2 | 13.2 | 13.2 | 13.2 |
| Monomer 'F' | 6.2 | 12.4 | 18.8 | 0.0 |
| | | | | |
| Initiator | | | | |
| Ammonium persulfate | 2.2 | 2.2 | 2.2 | 2.2 |
| Deionized water | 22.0 | 22.0 | 22.0 | 22.0 |
| | | | | |
| Chaser | | | | |
| Sodium metabisulfite | 0.4 | 0.4 | 0.4 | 0.4 |
| Deionized water | 3.0 | 3.0 | 3.0 | 3.0 |
| t-Butyl hydroperoxide | 0.4 | 0.4 | 0.4 | 0.4 |
| Deionized water | 3.0 | 3.0 | 3.0 | 3.0 |
| | | | | |
| Ammonium hydroxide | 2.1 | 2.1 | 2.1 | 2.1 |
| Adipic dihydrazide | 6.8 | 6.8 | 6.8 | 6.8 |
| Total | 650.9 | 650.1 | 651.5 | 650.7 |

Example 20

The latexes synthesized in examples 18 and 19 were formulated into semi-gloss coatings as per the following recipe.

| Grind | Pounds | Gallons |
|---------------------|----------------|---------------|
| Water | 100.00 | 12.00 |
| Natrosol® Plus 330 | 2.00 | 0.17 |
| Potassium carbonate | 2.50 | 0.13 |
| Tamol® 2001 | 6.25 | 0.68 |
| Drewplus® L-475 | 2.00 | 0.26 |
| Triton® CF-10 | 1.00 | 0.11 |
| Kathon® LX 1.5% | 1.50 | 0.18 |
| Ti-Pure® 706 | 230.00 | 6.90 |
| Minugel® 400 | 5.0 | 0.25 |
| Water | 80.00 | 9.60 |
| Total | 430.25 | 30.30 |
| Letdown | | |
| Water | 138.00 | 16.57 |
| Drewplus® L-475 | 2.00 | 0.26 |
| Strodex® PK | 4.00 | 0.44 |
| Drewthix® 864 | 1.00 | 0.11 |
| Drewthix 4025 | 10.00 | 1.15 |
| Latex | 469.00 | 53.30 |
| Total | 1054.25 | 102.13 |

The coatings were evaluated for various properties, and the test results are listed in the following table.

| | Control | 2% Monomer 'F' | 4% Monomer 'F' | 6% Monomer 'F' |
|-------------------------|---------|-------------------|-------------------|-------------------|
| Stormer viscosity, KU | 94.7 | 93.8 | 93.4 | 97.9 |
| ICI viscosity, Poises | 0.70 | 0.55 | 0.43 | 0.40 |
| Gloss at 20° | 20.0 | 17.3 | 17.2 | 16.6 |
| Gloss at 60° | 58.1 | 56.4 | 56.3 | 55.3 |
| 1-day block resistance | 3.5 | 3.5 | 3.5 | 4.0 |
| 7-day block resistance | 4.0 | 5.0 | 5.0 | 5.0 |
| 1 week scrub resistance | 3039 | 2267 | 2354 | 1841 |

1
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Example 21

| Kettle Charge | |
|-------------------------------|---------------|
| Deionized water | 140.00 |
| | |
| Stage I | |
| Deionized water | 165.00 |
| Rhodafac® RS-710 | 22.40 |
| Ammonium bicarbonate | 2.80 |
| Methyl methacrylate | 98.56 |
| Butyl acrylate | 103.60 |
| Hydroxy ethyl acrylate | 14.00 |
| Silane | 28.00 |
| Monomer 'F' | 28.00 |
| Methacrylic acid | 8.40 |
| | 470.76 |
| | |
| Initiator | |
| Deionized water | 25.00 |
| Ammonium persulfate | 0.39 |
| <i>t</i> -Butyl hydroperoxide | 0.76 |
| | |
| Deionized water | 25.50 |
| Bruggolite® FF6 | 0.65 |
| | |
| Chaser | |
| <i>t</i> -Butyl hydroperoxide | 0.12 |
| Deionized water | 5.00 |
| Bruggolite FF6 | 0.10 |
| Deionized water | 5.00 |
| | |
| Total | 673.29 |

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